

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

In re application of:

HAREN S. GANDHI ET AL.

Serial No.: 10/065,470

Filed: October 22, 2005

For: CATALYST SYSTEM FOR THE REDUCTION  
OF NO<sub>x</sub> AND NH<sub>2</sub> EMISSIONS

Group Art Unit: 1764

Examiner: Hien Thi Tran

Attorney Docket No.: FCHM 0119 PUS / 81045602

**APPEAL BRIEF UNDER 37 C.F.R. § 41.37**

Mail Stop Appeal Brief - Patents  
Commissioner for Patents  
U.S. Patent & Trademark Office  
P.O. Box 1450  
Alexandria, VA 22313-1450

Sir:

This is an Appeal Brief in support of the appeal from the final rejection of claims 1-31, 33, and 39 of the Office Action mailed on July 5, 2006 for the above-identified patent application.

**I. REAL PARTY IN INTEREST**

The real party in interest is Ford Global Technologies, L.L.C. ("Assignee"), a corporation organized and existing under the laws of the state of Delaware, and having a place of business at One Parklane Boulevard, Suite 600, Parklane Towers, East, Dearborn, Michigan as set forth in the assignment recorded in the U.S. Patent and Trademark Office on November 21, 2001 at Reel 013257/Frame 0219.

## **II. RELATED APPEALS AND INTERFERENCES**

There are no appeals or interferences known to the Appellants, the Appellants' legal representative, or the Assignee which will directly affect or be directly affected by or have a bearing on the Board's decision in the pending appeal.

## **III. STATUS OF CLAIMS**

Claims 1-31 and 33-39 are pending in this application. Claims 36-38 have been withdrawn from consideration. Claim 34 has been cancelled. Claims 24-29 and 39 are being cancelled herewith. Claims 1-23, 30-33 and 35 have been rejected and are the subject of this appeal.

## **IV. STATUS OF AMENDMENTS**

No response after final rejection has been filed.

## **V. SUMMARY OF CLAIMED SUBJECT MATTER**

The subject matter pertains to a catalyst system to facilitate the reduction of nitrogen oxides ( $\text{NO}_x$ ) and ammonia ( $\text{NH}_3$ ) from an exhaust gas, especially exhaust gases produced by an engine operating under lean air/fuel conditions (a ratio that is greater than the stoichiometric ratio of 14.6).

As a result of increasingly stringent fuel economy and emission standards for car and truck applications, it is preferable to operate an engine under lean air/fuel ratios. While lean operation improves fuel economy, operating under lean conditions increases the difficulty in treating some polluting gases, especially  $\text{NO}_x$ . For  $\text{NO}_x$  reduction under lean conditions, lean  $\text{NO}_x$  adsorber (trap) technologies have been widely utilized.

Lean  $\text{NO}_x$  adsorbers operate in a cyclic fashion of lean and rich durations. The lean  $\text{NO}_x$  trap functions by adsorbing  $\text{NO}_x$  when the engine is running under lean conditions

– until the NO<sub>x</sub> trap reaches the effective storage limit – followed by NO<sub>x</sub> reduction when the engine is running under rich conditions. During this rich cycle, a short rich pulse of reductants, carbon monoxide, hydrogen and hydrocarbons reduces the NO<sub>x</sub> adsorbed by the trap during the lean cycle. The reduction caused during the rich cycle purges the lean NO<sub>x</sub> adsorber, and the lean NO<sub>x</sub> adsorber is then immediately available for the next lean NO<sub>x</sub> storage/rich NO<sub>x</sub> reduction cycle. Lean NO<sub>x</sub> traps, however, often have the problem of low NO<sub>x</sub> conversion; that is, a high percentage of the NO<sub>x</sub> slips through the trap. (Page 2, ll. 6-33.)

NO<sub>x</sub> slip can occur either during the lean portion of the cycle or during the rich portion of the cycle. Lean NO<sub>x</sub> slip is often called “NO<sub>x</sub> breakthrough.” It occurs during extended lean operation and is related to saturation of the NO<sub>x</sub> trap capacity. Rich NO<sub>x</sub> slip is often called a “NO<sub>x</sub> spike.” It occurs during the short period in which the NO<sub>x</sub> trap transitions from lean to rich and is related to the release of stored NO<sub>x</sub> without reduction. Test results depicted in Figure 1a have shown that during this lean-rich transition, NO<sub>x</sub> spikes, the large peaks of unreacted NO<sub>x</sub>, accounts for approximately 73% of the total NO<sub>x</sub> emitted during the operation of a lean NO<sub>x</sub> trap. NO<sub>x</sub> breakthrough accounts for the remaining 27% of the NO<sub>x</sub> emitted. (Page 1, l. 31 - page 2, l. 13.)

An additional problem with lean NO<sub>x</sub> traps arise as a result of the generation of ammonia by the lean NO<sub>x</sub> trap. As depicted in Figure 1b, ammonia is emitted into the atmosphere during rich pulses of the lean NO<sub>x</sub> adsorber but the NO<sub>x</sub> conversion problem is magnified for diesel vehicles, which require more than a 90% NO<sub>x</sub> conversion rate under the 2007 U.S. Tier II BIN 5 Emission Standards at temperatures as low as 200°C. While high NO<sub>x</sub> activity is possible at 200°C, it requires extreme measures such as shortening the lean time, lengthening the rich purge time, and invoking very rich air/fuel ratios. All three of these measures, however, result in an increased formation of ammonia. Accordingly, while it may be possible to achieve 90+ % gross NO<sub>x</sub> conversion (the percentage of NO<sub>x</sub> that is reduced to

N<sub>2</sub>, N<sub>2</sub>O and NH<sub>3</sub>), there has not been a viable solution to achieve 90+ % net NO<sub>x</sub> conversion (the percentage of NO<sub>x</sub> that is reduced to nitrogen, N<sub>2</sub>, only).

Accordingly, a catalyst system that (1) reduces NO<sub>x</sub> breakthrough and NO<sub>x</sub> spikes from a lean NO<sub>x</sub> trap; (2) improves net NO<sub>x</sub> conversion; and (3) reduces NH<sub>3</sub> emissions would be useful. As a result, in the claimed catalyst system, net NO<sub>x</sub> conversion is improved and ammonia emissions reduced through the use of a lean NO<sub>x</sub> trap that is modified to optimize ammonia generation and a NH<sub>3</sub>-SCR catalyst system, which operates together to produce and store ammonia and reduce NO<sub>x</sub> to nitrogen.

Claim 1 recites an emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions from an exhaust gas stream, which includes a lean NO<sub>x</sub> trap in communication with the exhaust stream, wherein the lean NO<sub>x</sub> trap is optimized for NH<sub>3</sub> generation by removing oxygen storage capacity of the lean NO<sub>x</sub> trap. The emission control system also includes an NH<sub>3</sub>-SCR catalyst in communication with the exhaust stream for adsorbing the NH<sub>3</sub> generated by the lean NO<sub>x</sub> trap, so it can then react with NO<sub>x</sub> in the exhaust stream during lean conditions to improve net NO<sub>x</sub> conversion and reduce ammonia emissions.

Claim 20 recites an emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions that includes a lean NO<sub>x</sub> trap in communication with the exhaust stream, wherein the lean NO<sub>x</sub> trap comprises a lean NO<sub>x</sub> trap formulation which includes one or more NO<sub>x</sub> storage and NH<sub>3</sub> generating materials; and a NH<sub>3</sub>-SCR catalyst in communication with the exhaust stream for adsorbing NH<sub>3</sub>, wherein the NH<sub>3</sub>-SCR catalyst comprises a NH<sub>3</sub>-SCR catalyst formulation which includes one or more NH<sub>3</sub> adsorbing materials; and wherein the lean NO<sub>x</sub> trap formulation and the NH<sub>3</sub>-SCR catalyst formulation are placed on one substrate.

Claim 30 recites an emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions that comprises a lean NO<sub>x</sub> trap in communication with the exhaust stream to provide

a NO<sub>x</sub> reducing exhaust stream including NO<sub>x</sub> and NH<sub>3</sub>, wherein the lean NO<sub>x</sub> trap is optimized for NH<sub>3</sub> generation by removing oxygen storage capacity; and an NH<sub>3</sub>-SCR catalyst is also included in communication with the exhaust stream for adsorbing NH<sub>3</sub>, so that the NH<sub>3</sub> adsorbed by the NH<sub>3</sub>-SCR catalyst reacts with NO<sub>x</sub> to improve the reduction of NO<sub>x</sub> and NH<sub>3</sub>.

## **VI. GROUNDS OF REJECTION TO BE REVIEWED ON APPEAL**

Claims 1, 9-12, 14-17, 19, 30-31 and 33 stand rejected under 35 U.S.C. § 102(b) as being anticipated by Kinugasa et al. (U.S. Patent No. 6,109,024).

Claims 2-8, 18 and 20-23 stand rejected under 35 U.S.C. § 103(a) as being unpatentable over Kinugasa et al. (U.S. Patent No. 6,109,024) in view of Fuwa et al. (U.S. Patent No. 6,345,496).

Finally, claims 13 and 35 stand rejected under 35 U.S.C. § 103(a) as being unpatentable over Kinugasa et al. (U.S. Patent No. 6,109,024) in view of Yamada et al. (U.S. Patent No. 6,221,804).

## **VII. ARGUMENT**

### **A. Claims 1, 9-12, 14-17, 19, 30-31 And 33 Are Patentable Under 35 U.S.C. § 102(b) Over Kinugasa et al. (U.S. Patent No. 6,109,024)**

Kinugasa describes an emission control device that includes the adjustment of the lean to rich air/fuel ratio of the exhaust gas by a fuel injection technique to convert some NO<sub>x</sub> to NH<sub>3</sub>, which can be accomplished by a three way catalyst or a NO<sub>x</sub> adsorbing-reducing catalyst. (Col. 3, ll. 11-42.) More specifically, Kinugasa states that an exhaust gas with a rich air/fuel ratio which contains a relatively large amount of NO<sub>x</sub> is formed in the cylinder by direct cylinder fuel injection during the expansion or the exhaust stroke of the engine. (Col.

3, ll. 27-31.) Kinugasa then continues that “[t]his exhaust gas, having a rich air-fuel ratio and containing a relatively large amount of  $\text{NO}_x$ , is supplied to the  $\text{NH}_3$  conversion means such as a three way catalyst or a  $\text{NO}_x$  adsorbing-reducing catalyst. Since the amount of  $\text{NO}_x$  in the exhaust gas is large, a large amount of  $\text{NH}_3$  is produced by the  $\text{NH}_3$  conversion means and is supplied to the purification means. Therefore, a sufficient amount of  $\text{NH}_3$  for reducing  $\text{NO}_x$  in exhaust gas is supplied to the purification means.” (Col. 3, ll. 35-42.) In sum, Kinugasa relies on the creation of a rich air/fuel ratio to generate a large amount of  $\text{NO}_x$  in the exhaust gas which in turn would produce a large amount of  $\text{NH}_3$  when supplied to a three-way catalyst or a  $\text{NO}_x$  adsorbing-reducing catalyst.

In contrast, with the claimed subject matter, the lean  $\text{NO}_x$  trap itself is optimized for  $\text{NH}_3$  generation by removing oxygen storage capacity of the lean  $\text{NO}_x$  trap and thus  $\text{NH}_3$  is purposely generated by the lean  $\text{NO}_x$  trap for adsorption by the  $\text{NH}_3$ -SCR catalyst. This reservoir of adsorbed ammonia in the  $\text{NH}_3$ -SCR catalyst is then used to react directly with the  $\text{NO}_x$  emitted from the lean  $\text{NO}_x$  trap to improve overall net  $\text{NO}_x$  conversion — a rich air/fuel ratio does not need to be created. Kinugasa, however, never discloses any teaching to modify the lean  $\text{NO}_x$  trap to increase  $\text{NH}_3$  production and in turn improve net  $\text{NO}_x$  conversion.

The Examiner relies on Col. 8, ll. 37-43 and ll. 61-67 as evidence that Kinugasa discloses a lean  $\text{NO}_x$  trap that is optimized for  $\text{NH}_3$  generation by removing oxygen storage capacity. However, the cited lines state as follows:

On the other hand, when the oxygen concentration and the exhaust gas becomes low, i.e., when the excess air ratio  $\lambda$  of the exhaust gas becomes  $\lambda \leq 1.0$ , the production of  $\text{NO}_2$  on the surface of the platinum Pt is lowered and the reaction proceeds in an inverse direction ( $\text{NO}_3^- \rightarrow \text{NO}_2$ ), and thus nitric acid ions  $\text{NO}_3^-$  in the catalyst are released, in the form of  $\text{NO}_2$ , from the  $\text{NO}_x$  absorbing-reducing catalyst 7.

(Kinugasa, col. 8, ll. 37-43.)

In addition, the NO<sub>x</sub> adsorbing-reducing catalyst also converts NO<sub>x</sub> and the exhaust gas to NH<sub>3</sub> by a mechanism exactly the same as that of the three-way catalyst. Therefore, a NO<sub>x</sub> adsorbing-reducing catalyst can be used as the NH<sub>3</sub> conversion means in lieu of the three-way catalyst. Embodiments in which the NO<sub>x</sub> adsorbing-reducing catalyst is used as the NH<sub>3</sub> conversion means will be explained later.

(Kinugasa, col. 8, ll. 61-67.)

Nothing in the above quoted Kinugasa sections teach that the lean NO<sub>x</sub> trap should be modified by removing oxygen storage capacity to intentionally optimize NH<sub>3</sub> generation and in turn improve net NO<sub>x</sub> conversion.<sup>1</sup>

Kinugasa makes no mention of oxygen storage capacity or the use of a modified lean NO<sub>x</sub> trap to purposely increase NH<sub>3</sub> production. Accordingly, Kinugasa fails to teach the use of a lean NO<sub>x</sub> trap that has been enhanced for NH<sub>3</sub> production in combination with an NH<sub>3</sub>-SCR catalyst, and thus independent claims 1 and 30 along with dependent claims 9-12, 14-17, 19, 31 and 33 are allowable under 35 U.S.C. § 102(b) over Kinugasa et al.

**B. Claims 2-8, 18 And 20-23 Are Patentable Over Kinugasa, U.S. Patent No. 6,109,024, In View Of Fuwa et al., U.S. Patent No. 6,345,496**

As set forth above in reference to independent claim 1, as the Kinugasa et al. reference fails to disclose an emission system wherein the lean NO<sub>x</sub> trap is optimized for ammonia generation, dependent claims 2-8 and 18 are allowable for the reasons stated.

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<sup>1</sup> As is well known in the art, the amount of oxygen reversibly provided in and removed from the gas phase of a particular component is called oxygen storage capacity. Cerium oxide is a frequently used oxygen storing component, as are other materials such as NiO and FeO.

Independent claim 20 and the associated dependent claims 21-23, are patentable over Kinugasa and Fuwa et al. under the same rationale. Independent claim 20 specifically recites that the lean NO<sub>x</sub> trap is to be formulated to include NH<sub>3</sub> generating materials and thus the lean NO<sub>x</sub> trap itself is modified to optimize NH<sub>3</sub> generation so that the air/fuel ratio does not need to be adjusted to a rich one — as in Kinugasa.

Moreover, the Fuwa et al. reference teaches away from the claimed subject matter, as it requires the use of a three-way catalyst in contrast to the claimed subject matter wherein the lean NO<sub>x</sub> trap is specifically modified to generate NH<sub>3</sub> for subsequent reaction and conversion of NH<sub>3</sub> and NO<sub>x</sub>, as set forth in independent claims 1, 20 and 30. (Fuwa et al., col. 5, l. 52-Col. 6, l. 23.) As is well known in the art, for a traditional three-way catalyst if the air/fuel ratio is lean even by a small amount, NO<sub>x</sub> conversion drops to low levels. Accordingly, the Fuwa et al. reference teaches away from the claimed invention.

In addition, claims 4-8 are separately allowable as the claimed zoned structure has not been disclosed by the combination of Kinugasa et al. and Fuwa et al. In support of the rejection, the Examiner states that:

Fuwa discloses the conventionality of providing a control system in which the NO<sub>x</sub> trap and the NH<sub>3</sub>-SCR catalyst are alternating layers/zones in a single shell/substrate are mixed to form a single layer on one substrate. (Col. 25, l. 52; Col. 26, l. 7; Col. 27, ll. 13-23; Col. 30, l. 45-Col. 30, l. 6 in Figs. 39, 41a and 41b.)

(Office Action dated July 5, 2006.)

A review of the cited passages from Fuwa et al. reveals that the claimed alternating zoned structure in claims 4-8 is not disclosed.



Accordingly, for the reasons provided, claims 2-8, 18 and 20-23 are allowable under 35 U.S.C. § 103(a) over Kinugasa et al. in view of Fuwa et al.

**C. Claims 13 And 35 Are Patentable Over Kinugasa et al.  
In View Of Yamada et al. (U.S. Patent No. 6,221,804)**

As both claims 13 and 35 depend from independent claims 1 and 30, for the reasons set forth above in Section A, the combination of the Kinugasa and Yamada references does not teach an emission control system that uses a modified lean NO<sub>x</sub> trap to increase NH<sub>3</sub> production in combination with an NH<sub>3</sub>-SCR catalyst to reduce NH<sub>3</sub> emissions and improve net NO<sub>x</sub> conversion.

The fee of \$500 as applicable under the provisions of 37 C.F.R. § 41.20(b)(2) is enclosed. Please charge any additional fee or credit any overpayment in connection with this filing to our Deposit Account No. 06-1510.

Respectfully submitted,

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Enclosure - Appendices

### **VIII. CLAIMS APPENDIX**

1. An emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions from an exhaust stream, the system comprising:

a lean NO<sub>x</sub> trap in communication with the exhaust stream for reducing NO<sub>x</sub> emissions, wherein the lean NO<sub>x</sub> trap is optimized for NH<sub>3</sub> generation by removing oxygen storage capacity of the lean NO<sub>x</sub> trap; and

a NH<sub>3</sub>-SCR catalyst in communication with the exhaust stream for adsorbing NH<sub>3</sub>, wherein the NH<sub>3</sub> adsorbed by the NH<sub>3</sub>-SCR catalyst reacts with NO<sub>x</sub> in the exhaust stream to improve the reduction of NO<sub>x</sub> and NH<sub>3</sub>.

2. The emission control system of claim 1, wherein one or more alternating layers of the lean NO<sub>x</sub> trap and the NH<sub>3</sub>-SCR catalyst are provided in a single catalytic converter shell such that a top layer comprising the lean NO<sub>x</sub> trap positioned over a bottom layer comprising the NH<sub>3</sub>-SCR catalyst is repeated one or more times.

3. The emission control system of claim 1, wherein one or more alternating layers of the lean NO<sub>x</sub> trap and NH<sub>3</sub>-SCR catalyst are provided in a single substrate such that a top layer comprising the lean NO<sub>x</sub> trap positioned over a bottom layer comprising the NH<sub>3</sub>-SCR catalyst is repeated one or more times.

4. The emission control system of claim 1, wherein one or more alternating zones of the lean NO<sub>x</sub> trap and NH<sub>3</sub>-SCR catalyst are provided in a single catalytic converter shell such that an upstream zone comprising the lean NO<sub>x</sub> trap positioned upstream of a downstream zone comprising the NH<sub>3</sub>-SCR catalyst is repeated one or more times.

5. The emission control system of claim 4, wherein each alternating zone of the lean NO<sub>x</sub> trap and alternating zone of the NH<sub>3</sub>-SCR catalyst have a 1" length and 1" width.

6. The emission control system of claim 4, wherein each alternating zone of the lean NO<sub>x</sub> trap and alternating zone of the NH<sub>3</sub>-SCR catalyst have a ½" length and a width of ½".

7. The emission control system of claim 4, wherein each alternating zone of the lean NO<sub>x</sub> trap and alternating zone of the NH<sub>3</sub>-SCR catalyst have a length of ¼" and a width of ¼".

8. The emission control system of claim 1, wherein one or more alternating zones of the lean NO<sub>x</sub> trap and NH<sub>3</sub>-SCR catalyst are provided in a single substrate such that an upstream zone comprising the lean NO<sub>x</sub> trap positioned upstream of a downstream zone comprising the NH<sub>3</sub>-SCR catalyst is repeated one or more times.

9. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap generates a sufficient quantity of NH<sub>3</sub> to force the reaction between NO<sub>x</sub> and NH<sub>3</sub>, whereby NH<sub>3</sub> emissions are eliminated and net NO<sub>x</sub> conversion improved.

10. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap is optimized for NH<sub>3</sub> generation by removing oxygen storage capacity of the lean NO<sub>x</sub> trap.

11. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap comprises a precious metal selected from the group consisting of platinum, palladium, rhodium and combinations thereof; and a NO<sub>x</sub> storage material selected from the group consisting of alkali metals, alkali earth metals, rare earth metals and combinations thereof.

12. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap comprises platinum.

13. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap comprises a composite of cerium and zirconium.

14. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap comprises one or more materials for NH<sub>3</sub> generating and NO<sub>x</sub> storage.

15. The emission control system of claim 1, wherein the NH<sub>3</sub>-SCR catalyst comprises one or more NH<sub>3</sub> adsorbing materials, wherein the NH<sub>3</sub> adsorbing materials are capable of converting NO<sub>x</sub> and NH<sub>3</sub> to nitrogen.

16. The emission control system of claim 1, wherein the NH<sub>3</sub>-SCR catalyst comprises a base metal and a support selected from the group consisting of alumina, silica titania, zeolite and their combinations.

17. The emission control system of claim 1, wherein the NH<sub>3</sub>-SCR catalyst comprises a metal selected from the group consisting of Cu, Fe and Ce and a zeolite.

18. The emission control system of claim 1, wherein the lean NO<sub>x</sub> trap and the NH<sub>3</sub>-SCR catalyst are placed in a single catalytic converter shell.

19. The emission control system of claim 1, wherein the NH<sub>3</sub>-SCR catalyst is separate from and downstream from the lean NO<sub>x</sub> trap.

20. An emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions from an exhaust stream produced by the combination of an air/fuel mixture in an internal combustion engine, the system comprising:

a lean NO<sub>x</sub> trap in communication with the exhaust stream for NO<sub>x</sub> reduction wherein the lean NO<sub>x</sub> trap comprises a lean NO<sub>x</sub> trap formulation which includes one or more NO<sub>x</sub> storage and NH<sub>3</sub> generating materials;

a NH<sub>3</sub>-SCR catalyst in communication with the exhaust stream for adsorbing NH<sub>3</sub>, wherein the NH<sub>3</sub>-SCR catalyst comprises a NH<sub>3</sub>-SCR catalyst formulation which includes one or more NH<sub>3</sub> adsorbing materials; and

wherein the lean NO<sub>x</sub> trap formulation and the NH<sub>3</sub>-SCR catalyst formulation are placed on one substrate.

21. The emission control system of claim 20, wherein a layer of the lean NO<sub>x</sub> trap formulation and a layer of the NH<sub>3</sub>-SCR catalyst formulation are placed on the substrate to form a two-layer washcoat.

22. The emission control system of claim 20, wherein the lean NO<sub>x</sub> trap formulation and the NH<sub>3</sub>-SCR catalyst formulation are homogeneously mixed to form a single washcoat layer on the substrate.

23. The emission control system of claim 20, wherein the lean NO<sub>x</sub> trap formulation and the NH<sub>3</sub>-SCR catalyst formulation are heterogeneously mixed to form a single washcoat layer on the substrate.

30. An emission control system for controlling NO<sub>x</sub> and NH<sub>3</sub> emissions from an exhaust stream produced by the combination of an air/fuel mixture in an internal combustion engine, the system comprising:

a lean NO<sub>x</sub> trap in communication with the exhaust stream for NO<sub>x</sub> reduction, to provide a NO<sub>x</sub> reducing exhaust stream including NO<sub>x</sub> and NH<sub>3</sub>, wherein the lean NO<sub>x</sub> trap is optimized for NH<sub>3</sub> generation by removing oxygen storage capacity; and

a NH<sub>3</sub>-SCR catalyst in communication with the exhaust stream for adsorbing NH<sub>3</sub>, wherein the NH<sub>3</sub> adsorbed by the NH<sub>3</sub>-SCR catalyst reacts with NO<sub>x</sub> in the NO<sub>x</sub> reduced exhaust stream to improve the reduction of NO<sub>x</sub> and NH<sub>3</sub>.

31. The emission control system of claim 30, wherein the lean NO<sub>x</sub> trap generates a sufficient quantity of NH<sub>3</sub> to force the reaction between NO<sub>x</sub> and NH<sub>3</sub>, whereby NH<sub>3</sub> emissions are eliminated and net NO<sub>x</sub> conversion improved.

33. The emission control system of claim 30, wherein the lean NO<sub>x</sub> trap comprises a precious metal selected from the group consisting of platinum, palladium, rhodium and combinations thereof; and a NO<sub>x</sub> storage material selected from the group consisting of alkali metals, alkali earth metals, rare earth metals and combinations thereof.

35. The emission control system of claim 30, wherein the lean NO<sub>x</sub> trap comprises a composite of cerium and zirconium.

**IX. EVIDENCE APPENDIX**

None

**X. RELATED PROCEEDINGS APPENDIX**

None